

## **DEHYDRATION KINETICS OF AN INDIAN CLAY**

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Decomposition of clay from Garo Hills of Meghalaya (India) was studied by dynamic thermogravimetry. A fourteen kinetic equation procedure was applied for analysis of non-isothermal weight change upto a temperature of 1223 K. Two stages of decomposition were clearly distinguished i.e. the initial dehydration period at temperature 373 K to 673 K and the dehydroxylation period in the temperature range 723 K to 1073 K. First order decomposition mechanism was found to be applicable to both dehydration and dehydroxylation steps. Activation energies of 67 kJ/mol and 278 kJ/mol are estimated for the first and second steps with frequency factors of  $16.3 \text{ s}^{-1}$  and  $5.16 \times 10^6 \text{ s}^{-1}$  respectively. The weight loss relating to the steps in TG curves allows determination of the contents of the basic mineral in the clay. Percentages of  $\text{Al}_2\text{O}_3 \cdot \text{SiO}_2$  and total volatiles as calculated from weight loss data are in accordance with the results of classical chemical analysis.

This paper reports non-isothermal thermogravimetric analysis of the clay in the Garo Hill of Meghalaya (India) leading to the approximate estimate of the chemical constituents and important kinetic parameters.

A number of models have been developed for solid decomposition mechanism and methods have been worked out for solving the differential equation which could represent the decomposition of solids determined under isothermal and non-isothermal conditions. The retrieval of the kinetic parameters from the weight loss versus temperature data can be done by using one of several techniques such as those developed by Freeman and Carroll [1], Horowitz and Metzger [2], Gorbachev [3], MacCallum and Tanner [4], Coats and Redfern [5], and Reich and Stivala [6]. Other techniques are available for specific decomposition mechanisms such as those developed by Satava and Škvara [7] and Blazejowski [8]. Modified version of Coats and Redfern Technique [9] has been developed and found to be the easiest of all methods. This has further been modified to cover wide range of

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mechanistic model [10]. Terez [11] has proposed a procedure for a modified Freeman and Carroll method.

### Theoretical

The process of clay dehydroxylation may be described by a fundamental equation of non-isothermal kinetics. The ultimate aim of analysing dynamic TG curve is to linearize the data in the form of the decomposition fraction as a function of temperature, ( $T$ ). Certain well established kinetic solid-state equations are employed to describe the TG curve and are associated with one or more rate determining mechanism. In the present paper we adopt three methods using nine of the basic kinetic equations ( $D_1, D_2, D_3, D_4, F_1, A_2, A_3, R_2, R_3$ ). For all procedure of analysis, a least square fit for a straight line has been employed and the corresponding correlation co-efficient,  $r$  and standard error or deviation  $S_e$  were estimated.

*The following methods are used in this paper*

1) The method of Coats and Redfern (CR): In the original method [5], the authors assumed a first order reaction mechanism as well as fractional order down to zero.

In recent year, the method has been modified and extended to cover all of the nine currently accepted solid-state reaction mechanism [10]. The general equation is of the form:

$$\log \left[ \frac{g(\alpha)}{T^2} \right] = \log \left[ \frac{AR}{\Phi E_a} \right] - \frac{E_a}{2.3RT} \quad (1)$$

or

$$\log \left[ \frac{g(\alpha)}{T^2} \right] = \log \left[ \frac{AR}{\Phi E_a} \left( 1 - \frac{2RT}{E_a} \right) \right] - \frac{E_a}{2.3RT} \quad (2)$$

where,  $T$  is the absolute temperature at the specified fraction,  $R$  is the gas constant,  $E_a$  is activation energy,  $A$  is the Arrhenius frequency factor and  $\varphi$  is heating rate. If the correct  $g(\alpha)$  is used, a plot of the left hand side of the equation vs.  $1/T$  should give a straight line from which the values of  $E_a$  and  $A$  could be estimated.

2) The method of Blazejowski (Blz): This method was applicable to certain solid-state reaction kinetics [8]. The basic equation involved is

$$\log \frac{g(\alpha)}{T} = \log \frac{A}{\Phi} - \frac{E_a}{2.3RT} \quad (3)$$

which is found to be suitable in the linearized procedure. Values of  $E_a$  and  $A$  then can be evaluated easily.

3) The method of Satava and Škvara (SS): According to this method,  $\log g(\alpha)$  is plotted against  $1/T$  for each of the nine solid-state decomposition mechanism. From the slope of the best straight line, extending over the whole range of decomposition,  $E_a$  can be calculated from the approximate formulae:

$$E_a = -\tan\beta + \sqrt{\tan^2\beta + 8 \tan\beta \cdot T} \quad (4)$$

where  $\tan\beta$  is the slope of the straight line and  $T$  is the temperature corresponding to 50% decomposition.

## Experimental

Representative clay sample was ground to -325 mesh, washed in distilled water, decanted and dried before subjecting to DTA. TG, DTA and DTG were recorded with MOM (OD 103) derivatograph, taking 200 mg of clay sample. Reference samples was  $\alpha$ - $\text{Al}_2\text{O}_3$  and heating rate was 4.66 K per second in static  $\text{N}_2$  atmosphere.

## Results and discussion

Thermogravimetric curves are shown in Fig. 1. The TG curve shows clearly two distinct zones of dehydration. The first zone is indication of loss of water which is physically adsorbed on clay surfaces while the second zone is due to loss of structural water i.e. loss due to dehydroxylation. One may easily infer that the clay is basically of the kaolinitic ( $\text{Al}_2\text{Si}_2\text{O}_5(\text{OH})_4$ ) structure from which removal of hydroxyl takes place above 723 K, the peak temperature being obtained between 773 K to 873 K. The peak temperature

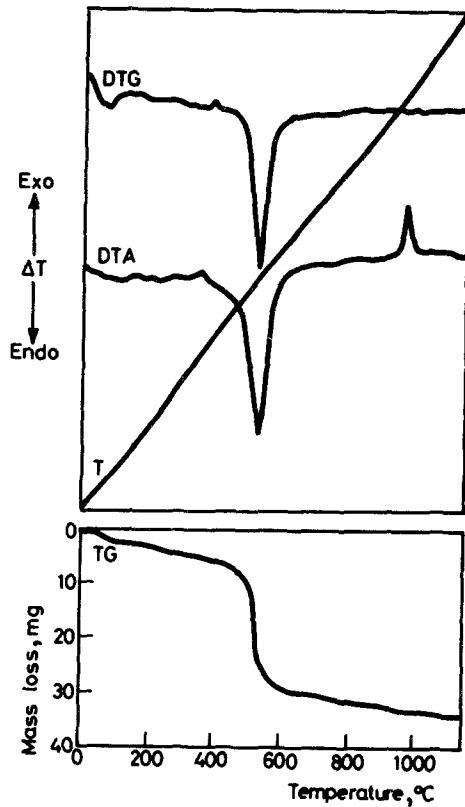


Fig. 1 TG, DTG, DTA curves of the clay

832 K obtained here with finely ground washed clay sample is thought to be representative of the clay, though in general peak temperature varies with impurities present, heating rate, water vapour pressure and other experimental conditions [12]. The first dehydration step is involved with a loss of about 4% water while the dehydroxylation step involved a loss of about 13% water which is almost equal to the percentage of structural water present in kaolin. From the initial mass of sample taken and the process of dehydration of single mineral and following a standard procedure [13], the kaolin content was found to be 92% which implies that  $\text{Al}_2\text{O}_3$  and  $\text{SiO}_2$  contents in the clay are 36.34% and 42.81% respectively. Chemical analysis of the clay shows an  $\text{Al}_2\text{O}_3$  content of 36.9% and  $\text{SiO}_2$  content of 44.56%. Thus

the thermoanalytical results show reasonable accuracy in supporting kaolin as the predominant nature of the clay.

The two dehydration steps are transferred into kinetic curves and shown as fractional decomposition (dehydration and or dehydroxylation) vs.

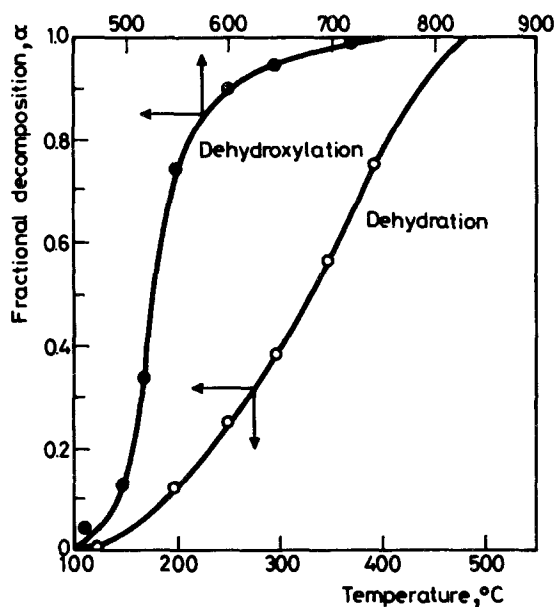


Fig. 2 Fraction decomposed as function of temperature

temperature. Table 1 shows the kinetic parameters namely  $E_a$  and  $A$  for the nine mechanistic model using all fourteen functions and the three methods mentioned earlier. The results pertain to the entire range of decomposition and statistical test for the goodness of fit was performed following a standard procedure [14] in a computer (HCl India, System IV). Both dehydration and dehydroxylation of the clay follow first order kinetic mechanism though there is some proximity to second order mechanism. Earlier workers have established first order kinetic mechanism for pure kaolin [15]. But some workers report a diffusion controlled reaction in vacuo. It may be believed that most observation of first order kinetics can be reinterpreted in accordance with a diffusion controlled mechanism. Pseudo phase boundary controlled mechanism was also proposed by some workers [16] with  $E_a$  and  $A$  values of 172.62 kJ/mole and  $14.85 \times 10^{10} \text{ s}^{-1}$  respectively.

Table 1 Kinetic parameters for clay dehydration / dehydroxylation. A. Initial dehydration period

Mechanism Method Notation	Biz method			CR method			SS method		
	$E_a$ , kJ/mol	$A_1$ , $s^{-1}$	$r$	$E_a$ , kJ/mol	$A_1$ , $s^{-1}$	$r$	$E_a$ , kJ/mol	$r$	$S_e$
1	56.13	0.51	-0.97	46.01	1.95	-0.96	187.60	-0.98	1.4
2	122.40	83.46	-0.98	112.30	773.40	-0.97	314.82	-0.98	2.79
3	11.96	0.017	-0.93	1.825	0.003	-0.33	72.17	-0.98	0.47
4	62.34	0.53	-0.986	55.21	0.02	-0.97	181.47	-0.99	1.21
5	64.59	0.46	-0.988	54.46	2.07	-0.98	160.70	-0.99	1.15
6	69.34	2.39	-0.942	59.20	11.72	-0.98	168.35	-0.99	1.02
7	42.85	0.26	-0.99	32.71	0.71	-0.98	112.41	-0.99	0.68
8	29.60	0.087	-0.986	19.47	0.14	-0.96	111.90	-0.99	0.51
9	16.36	-0.0289	-0.981	6.22	0.015	-0.85	57.21	-0.99	0.34
10	130.20	104.00	-0.986	120.10	$1.03 \times 10^3$	-0.98	320.72	-0.98	2.54
11	133.20	32.90	-0.98	123.10	$3.34 \times 10^2$	-0.98	302.57	-0.99	2.46
12	139.30	66.71	-0.99	129.20	$7.10 \times 10^2$	-0.99	339.18	-0.99	2.30
13	85.70	15.86	-0.994	75.57	98.92	-0.99	133.99	-0.99	1.38
14	77.13	2.95	-0.994	67.00	16.33	-0.99	212.15	-0.99	1.08

Table 1. Kinetic parameters for clay dehydration / dehydroxylation. B. Dehydroxylation period

Mechanism Method Notation	Blz method			CR method			SS method		
	$E_a$ , kJ/mol	$A_1$ , s <sup>-1</sup>	$r$	$E_a$ , kJ/mol	$A_1$ , s <sup>-1</sup>	$r$	$E_a$ , kJ/mol	$r$	$S_e$
1	132.50	9.74	-0.812	116.20	58.61	-0.772	349.60	-0.844	4.24
2	281.30	$4.75 \times 10^4$	-0.829	265.00	65.00	-0.812	490.60	-0.844	8.49
3	33.32	0.034	-0.72	17.045	0.0298	-0.463	154.49	-0.844	1.41
4	168.90	63.31	-0.862	152.70	500.30	-0.836	423.92	-0.882	4.51
5	184.60	125.40	-0.879	168.30	$1.09 \times 10^3$	-0.858	455.64	-0.896	4.56
6	222.00	$5.03 \times 10^3$	-0.912	205.70	$5.3 \times 10^4$	-0.898	531.43	-0.923	4.59
7	142.65	36.98	-0.905	126.30	241.71	-0.882	370.22	-0.923	3.06
8	102.90	3.167	-0.898	86.59	14.21	-0.862	288.77	-0.923	2.29
9	63.15	0.2789	-0.882	46.88	0.66	-0.807	266.04	-0.923	1.53
10	322.10	$4.3 \times 10^5$	-0.853	305.90	$6.8 \times 10^6$	-0.840	733.29	-0.865	8.90
11	342.30	$3.91 \times 10^5$	-0.865	326.00	$6.6 \times 10^6$	-0.854	773.80	-0.876	8.99
12	385.40	$7.88 \times 10^6$	-0.888	369.10	$1.5 \times 10^8$	-0.879	860.50	-0.896	9.12
13	382.90	$3.16 \times 10^3$	-0.954	366.67	$5.9 \times 10^9$	-0.972	850.40	-0.977	4.09
14	294.20	$3.6 \times 10^5$	-0.974	277.90	$5.16 \times 10^6$	-0.98	720.55	-0.956	4.43

The values of activation energy found out by SS method were considerably higher than those obtained by the other two methods for all the fourteen equations. This is reasonable since the sensitivity of SS method is relatively lower though it offers useful kinetic information in general [17]. The CR method gives smallest values of  $E_a$  for both the steps involved while Blz method gives values lying inbetween. However, Blz method reveals that the straight line fit is better for all fourteen mechanism in both the dehydration and dehydroxylation steps. Recent finding is that CR method extended to any  $g(\alpha)$  is the most reliable method for non-isothermal analysis [18]. In the present case also, CR method shows better correlation ( $r = .98$  and  $S_e = 17 \times 10^{-2}$ ) for the first order mechanism resulting in  $E_a$  values of 67 kJ/mole and 278 kJ/mole for dehydration and dehydroxylation steps with corresponding  $A$  values of  $16.3 \text{ s}^{-1}$  and  $5.16 \times 10^6 \text{ s}^{-1}$  respectively while Blz method shows  $E_a$  values of 77 and 294 kJ/mole for the two steps with  $A$  values of  $3 \text{ s}^{-1}$  and  $4 \times 10^5 \text{ s}^{-1}$  respectively ( $r = .994$ ,  $S_e = 18 \times 10^{-3}$  for dehydration and  $r = 0.974$ ,  $S_e = 3.49 \times 10^{-1}$  for dehydroxylation).

Since kinetic law for kaolin dehydroxylation is reported to change at a conversion degree of greater than 60% [19], regression analysis was separately performed using data on conversion below 60%. Better correlation was obtained for the proposed mechanism using CR technique, the values of  $E_a$  and  $A$  being 262.1 kJ/mole and  $4.01 \times 10^6 \text{ s}^{-1}$  respectively ( $r = .992$  and  $S_e = 7 \times 10^{-3}$ ). The value of  $E_a$  calculated for the clay is higher than those for natural, synthetic as well as activated kaolin reported recently [20]. However, wide variation in  $E_a$  value (i.e. 200 to 840 kJ/mole) is possible depending on the sources of kaolin [21]. The value of  $A$  for the dehydroxylation step obtained in this work is significantly lower in comparison to figures in the range of 7.6 to  $14.8 \times 10^{10} \text{ s}^{-1}$  reported in literature [16]. The observed variation may be attributed to differences in structural properties, particle size, particle packing in aggregate and the size and density of the aggregate of clay. However, the observed results would be quite reasonable for industrial design of calcination process.

## Conclusion

1) Analysis of non isothermal thermogravimetric curves of an indian clay upto temperature of 1223 K revealed two stages of dehydration i.e. an initial dehydration period at temperature 373 K to 673 K and a dehydroxylation period in the temperature range 723 K to 1073 K.



2) First order decomposition mechanism was found to be predominant to both dehydration and dehydroxylation steps which are associated with activation energies of 67 kJ/mol and 278 kJ/mol respectively. The corresponding values of the frequency factor are  $16.3s^{-1}$  and  $5.16 \times 10^6 s^{-1}$  respectively.

3) Analysis of the weight loss relating to steps in TG curves further reveals that the clay is basically kaolinitic in nature and that the  $Al_2O_3$  and  $SiO_2$  contents of the clay are 36.34% and 42.81% respectively which are comparable to the values of 36.9% and 44.56% as obtained by classical chemical analysis.

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**Zusammenfassung** – Mittels DTG wurde die thermische Zersetzung von Ton aus der Garo-Hills-Gegend bei Meghalaya (Indien) untersucht. Zur Analyse der nicht-isothermen Gewichtsveränderungen bis zu einer Temperatur von 1223 K wurde ein Verfahren mit vierzehn kinetischen Gleichungen angewendet. Zwei Teilschritte der Zersetzung können eindeutig unterschieden werden, nämlich die anfängliche Dehydratationsperiode bei Temperaturen von 373 bis 673 K und die Dehydroxylierungsperiode bei Temperaturen zwischen 723 K und 1073 K. Für beide Vorgänge konnte als Reaktionsmechanismus eine Zersetzung erster Ordnung angewendet werden. Für den ersten und zweiten Teilschritt konnten Aktivierungsenergien von 67 kJ/mol bzw. 278 kJ/mol und Frequenzfaktoren von  $16.3s^{-1}$  bzw.  $5.16 \times 10^6 s^{-1}$  ermittelt werden. Der aus den TG-Kurven hervorgehende Gewichtsverlust läßt auf den Gehalt des Tones an Basismineral schließen. Der prozentuelle Gehalt an  $Al_2O_3$ ,  $SiO_2$  und der gesamten flüchtigen Bestandteile, berechnet aus den Gewichtsverlustraten, stimmt mit den Ergebnissen aus herkömmlichen chemischen Analysen überein.